

Butanol Fermentation from Low-Value Sugar-Based Feedstocks by *Clostridia*

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2012.9.10

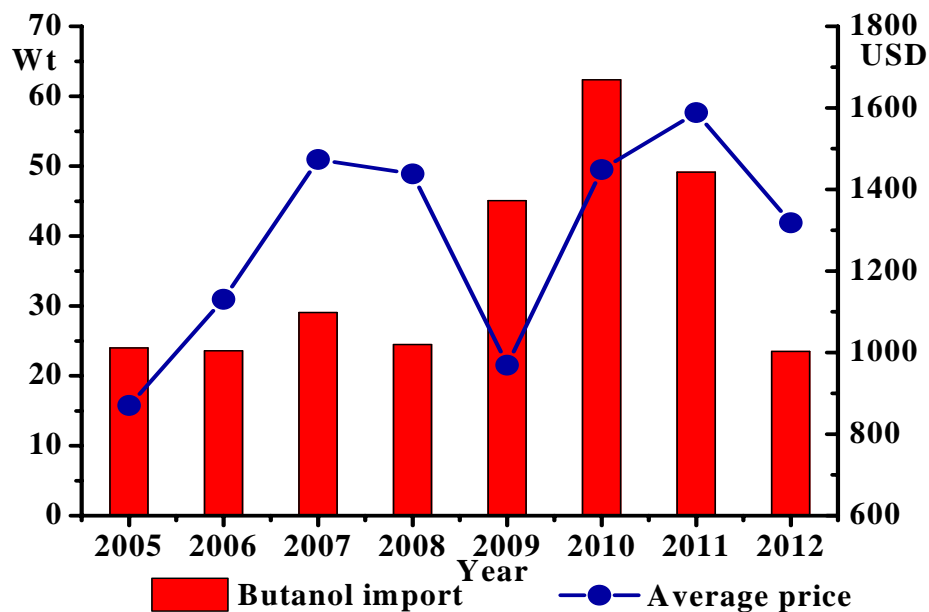
Current Status of Bio-butanol in China

- **Market**
- **Factories**
- **Research**

Studies on ABE fermentation in Our Lab

- **Continuous Fermentation by *Clostridium saccharobutylicum***

Butanol consumption and import in China



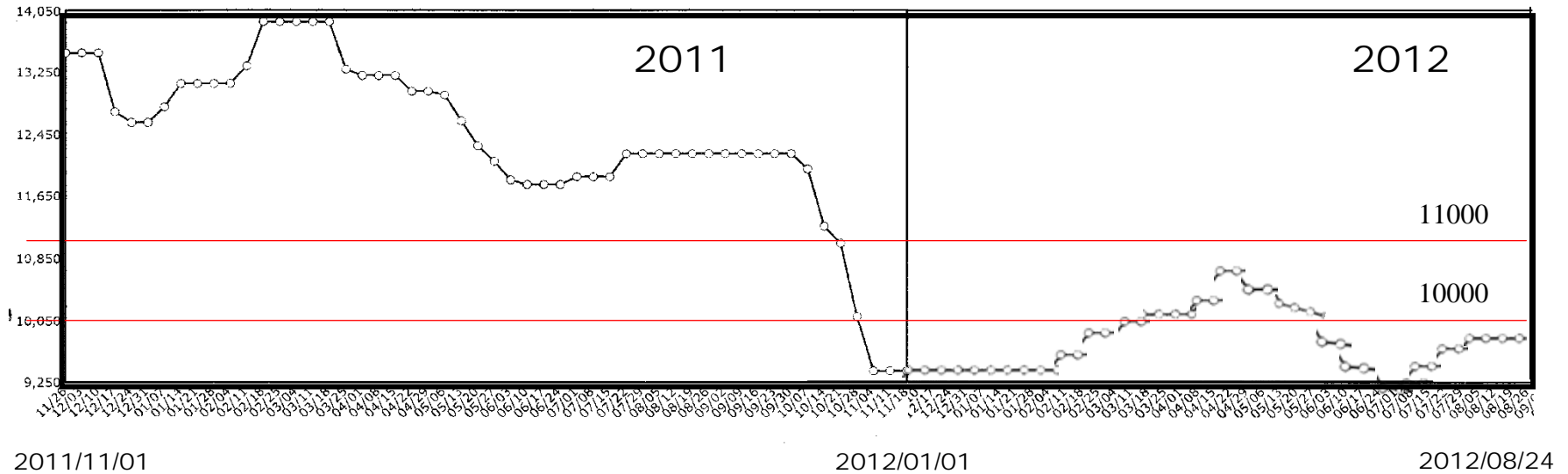
Year	Butanol import	Average price
	Ton	USD
2005	239926	870.5
2006	235834	1130.6
2007	290358	1473.6
2008	244661	1438.4
2009	450742	968.9
2010	623509	1448.9
2011	491246	1588.2
2012.1-6	235083	1318.5

During the period of 2005–2011, around **50%** of total annual butanol consumption was imported, and butanol consumption increased rapidly at an average rate of **6-8%** in China.

(Data sources : <http://chem.chem99.com/>)

Butanol Price Trend in China

Butanol Price (Jilin Petrochemical)



(<http://jiage.china.alibaba.com/price/trend/>)

Market: butanol price downturn continuation ...

Factories

ABE Factories in China (data by 2012.8)

Factory	Current Capacity (t/y)	Starting date	Current Status	Address
Laihe Rockley Bio-Chemicals Ltd	150,000	2007.12.5	–	Songyuan, Jilin
Jilin Cathay Biotechnology Co. Ltd	100,000	2008.3.20	–	Jilin, Jilin
Guangxi Guiping JinYuan Alcohol Co. Ltd	30,000	2007.8	–	Guiping, Guangxi
Jimaoyuan Biochemical Co. Ltd	40,000	2008.3.2	producing ethanol	Lianyungang, Jiangsu
Lianhai Biological Co. Ltd	50,000	2008.10	–	Haimen, Jiangsu
Lianyungang Union of Chemicals Co. Ltd	40,000	2010.4	producing ethanol	Lianyungang, Jiangsu

All ABE factories stopped production or switch to ethanol ...



Research

Choice of Feedstocks for ABE Fermentation

Starchy materials:

corn, **cassava**, wheat

Molasses:

cane and beet molasses

Cellulosic biomasses:

crop straw hydrolysate

Energy crops:

sweet sorghum, jerusalem artichoke



Food materials



Substitutes



**Low-value
sugar-based
feedstocks**

Cost issue

“Food versus fuel” debate

Corn material

Profit from corn utilization in ABE fermentation in China

Utilization of corn components (per ton corn)

Corn components	Output (Kg)	Price (Yuan/t)	Profits (Yuan)
Starch (10% water)	600	2860	1700
Fiber	115~120	1350	160~200
Embryo	50~60	4500	270
Protein	60	4300	250
CSL (45% water)		350	
Total			2420

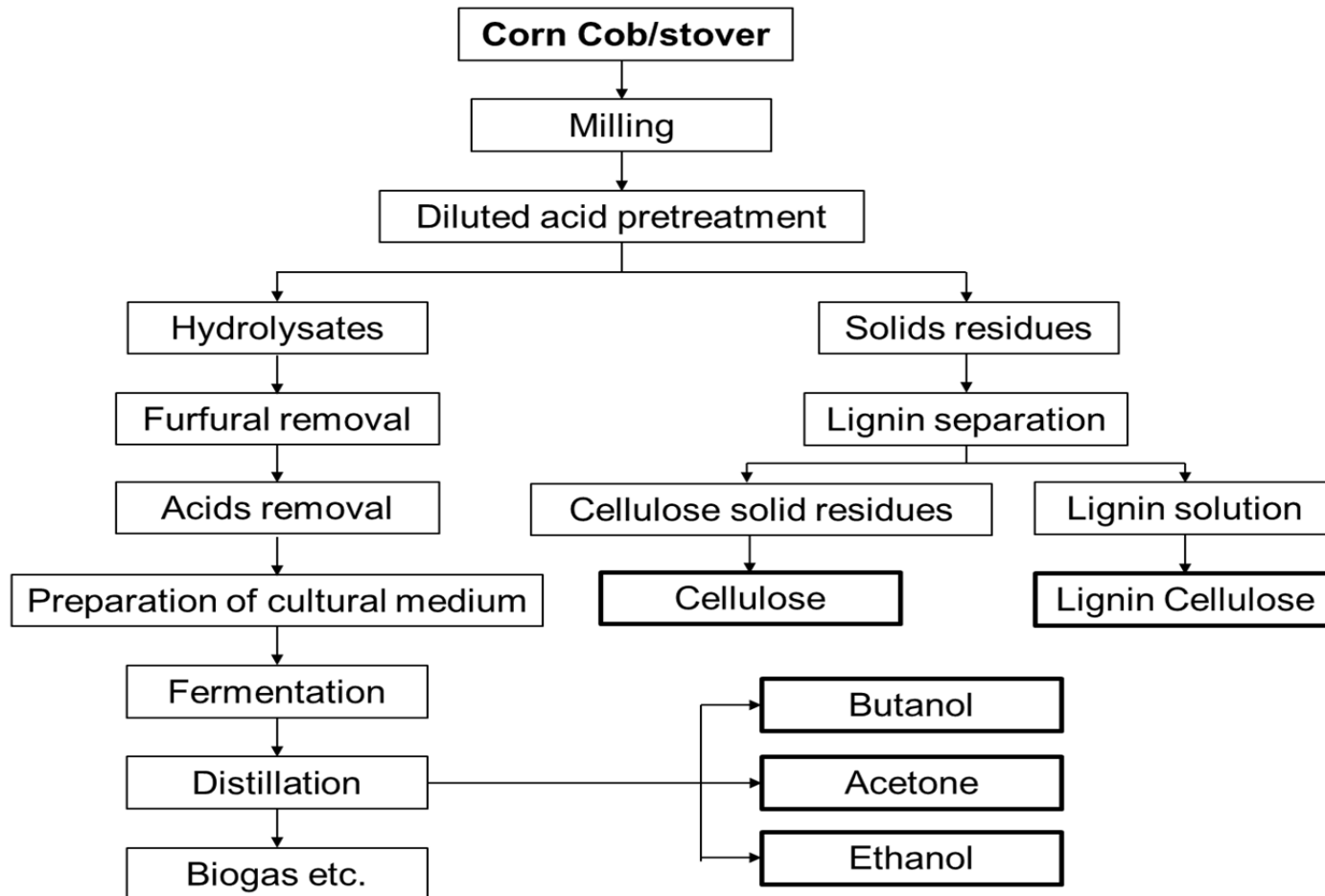
} **720**

*CSL: 10% solid content (3% protein), its profit was not considered.

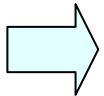
- In 2012.2, corn price in Jilin is **2,030 yuan/t** (14% water), including shipping;
- 4.5~4.7 t corn/t solvent, equal to a material cost of **10,080 yuan/t solvent**;
- After utilization of corn component: **3,200 yuan/t solvent**, the material cost: **7,000 yuan**.

Corn Stover material

Corn Stover Butanol Biorefinery



Corn Stover Butanol Biorefinery



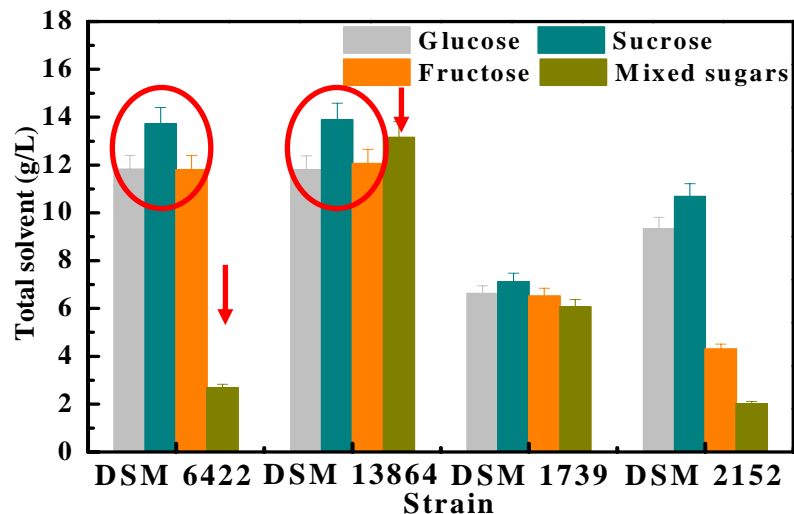
Corn stover cost when construction: 200 yuan/t; when production: 500–700 yuan/t

Studies on ABE in Our Lab

Continuous Butanol Fermentation from Low-Value Sugar-Based Feedstocks by *Clostridium saccharobutylicum* DSM13864

Sugar Utilization of *Clostridial* Strains

Sugars utilization of various *Clostridial* strains in ABE fermentation



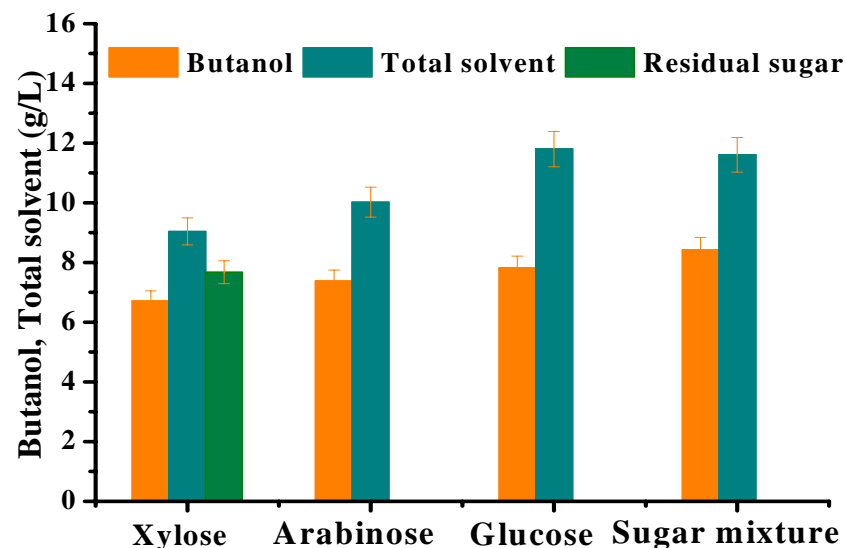
C. Beijerinckii DSM 6422、DSM 1739

C. Saccharobutylicum DSM 13864

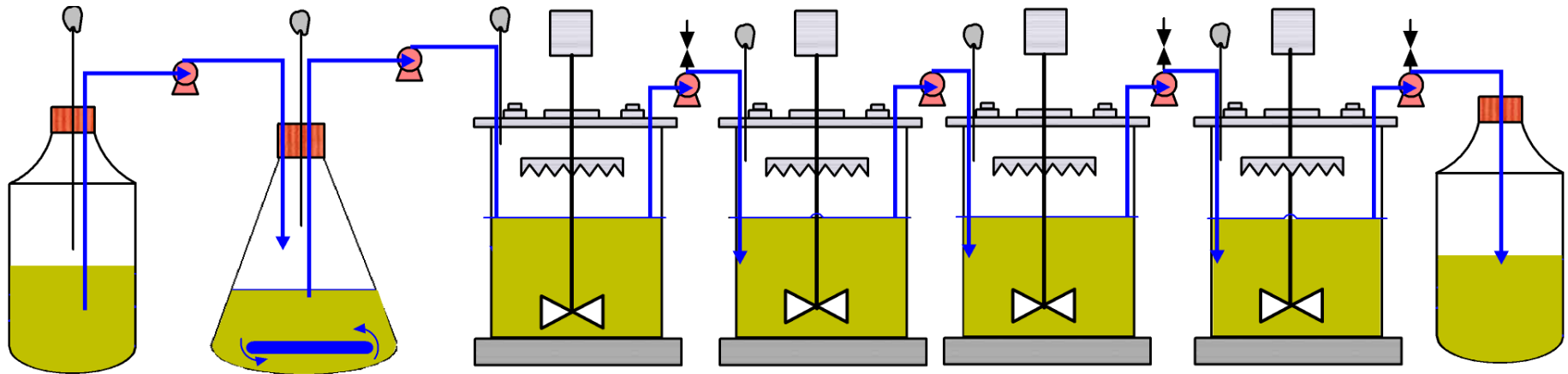
C. Saccharoperbutylacetonicum DSM 2152

C. saccharobutylicum DSM 13864
could be used for ABE fermentation
from cane molasses.

C. saccharobutylicum DSM 13864
could be used for ABE fermentation
from lignocellulosic hydrolysates.



Scheme of 4-Stage Continuous ABE fermentation

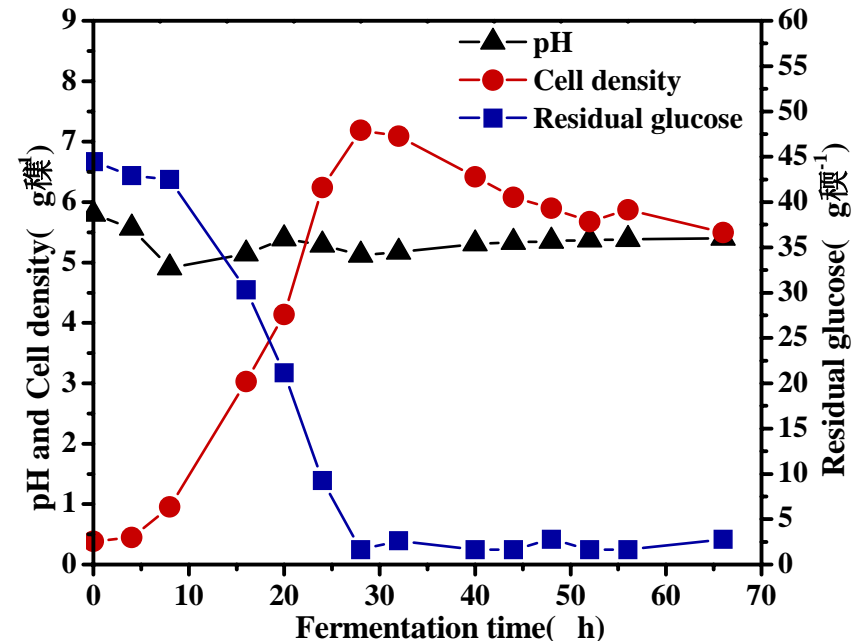
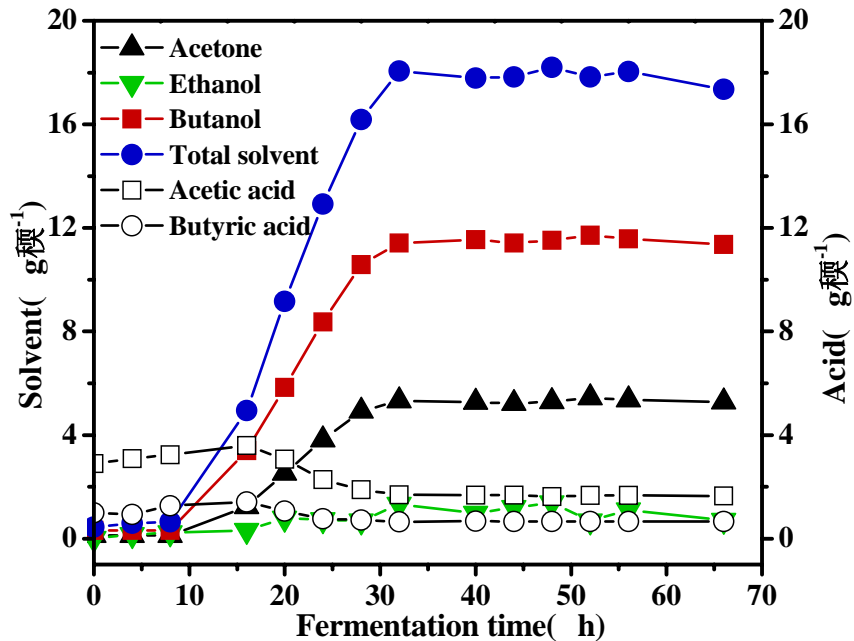


Feeding tank Blending vessel Bioreactor 1 Bioreactor 2 Bioreactor 3 Bioreactor 4 Collection tank

Substrate: **glucose**

Strain: **DSM 13864**

Batch fermentation in 3-L bioreactor



Total solvent: 18.20 g/L (butanol 11.53 g/L)

Productivity: 0.379 g/L/h

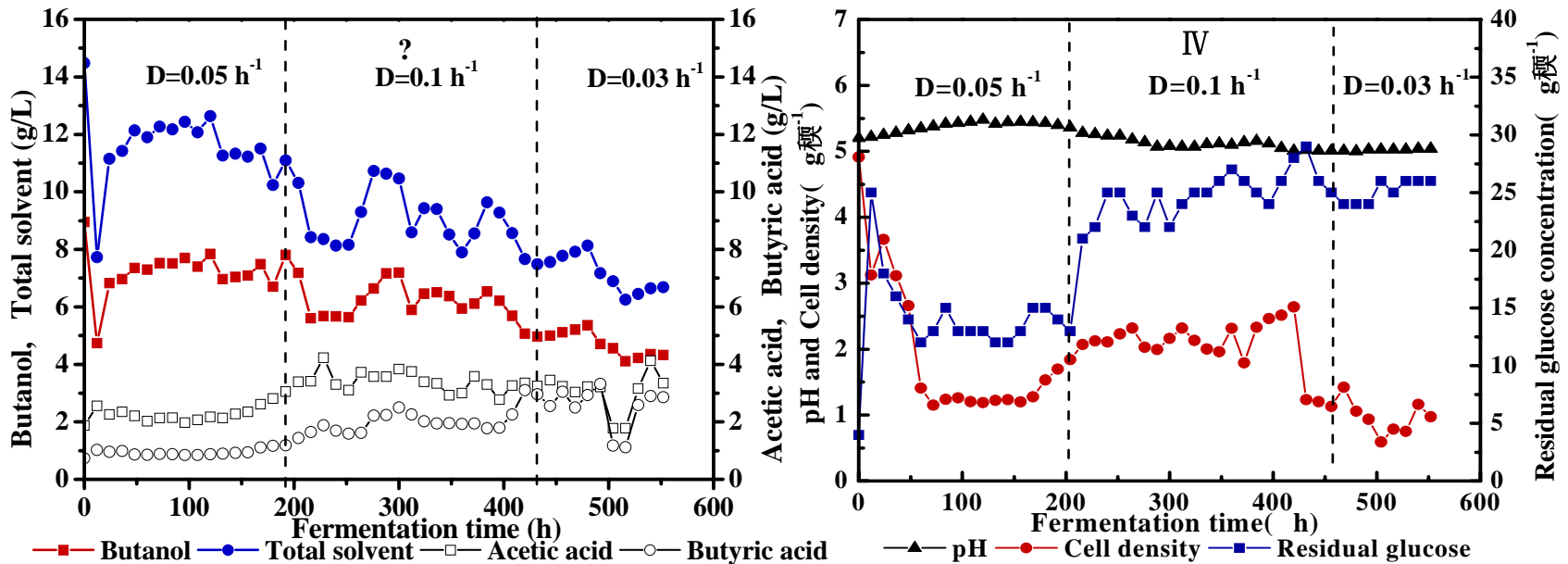
Yield: 0.314 g ABE/g sugar

Fermentation time: 48 h

Substrate: glucose

Strain: DSM 13864

4-Stage continuous fermentation ($D=0.03, 0.05, 0.1 \text{ h}^{-1}$)



At $D = 0.05 \text{ h}^{-1}$:

Total solvent: 11.57 g/L (butanol 7.29 g/L); Productivity: 0.145 g/L/h

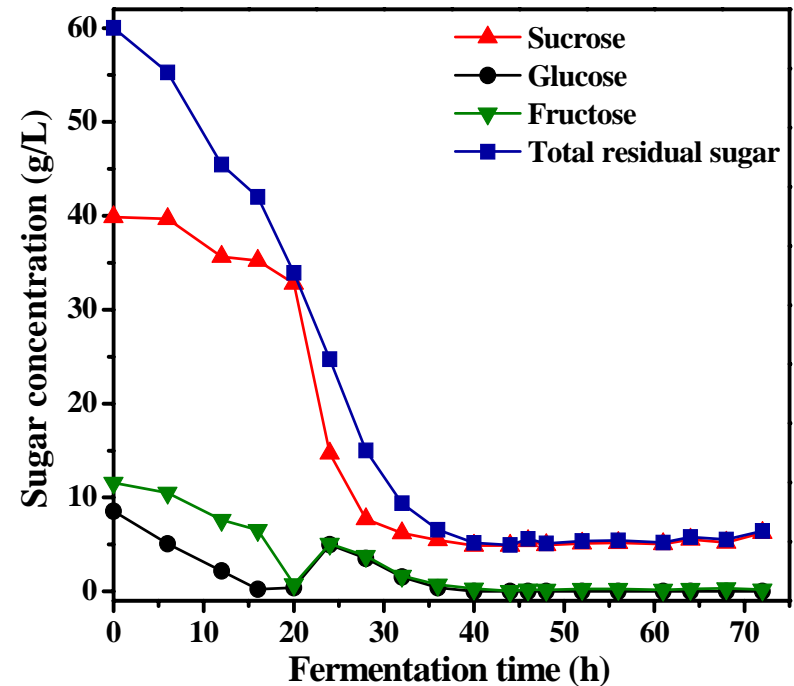
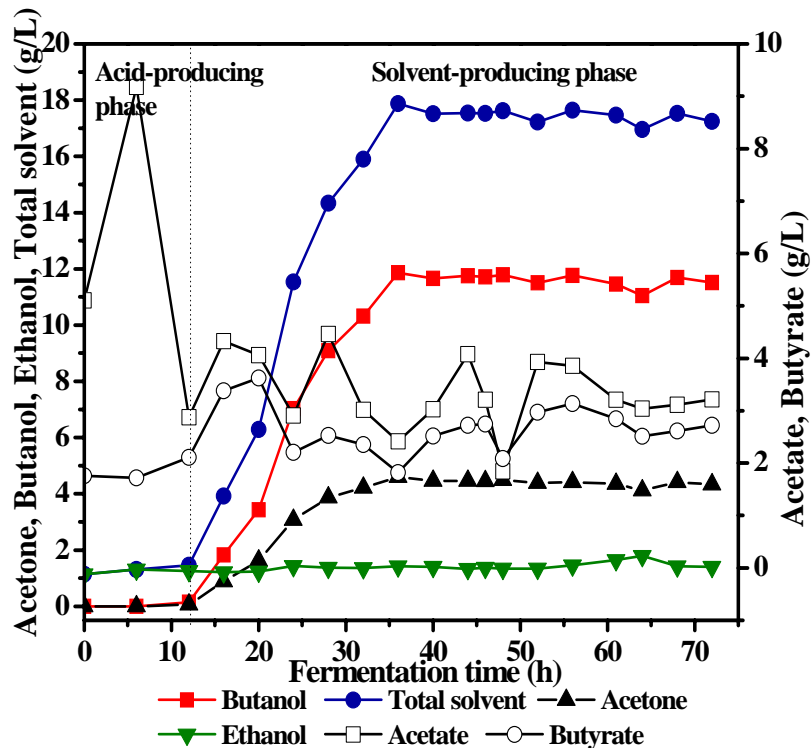
At $D = 0.1 \text{ h}^{-1}$:

Total solvent: 8.99 g/L (butanol 6.14 g/L); Productivity: 0.225 g/L/h

Substrate: cane molasses

Strain: DSM 13864

Batch fermentation in 5-L bioreactor



Total solvent: 17.88 g/L (butanol 11.86 g/L)

Productivity: 0.50 g/L/h

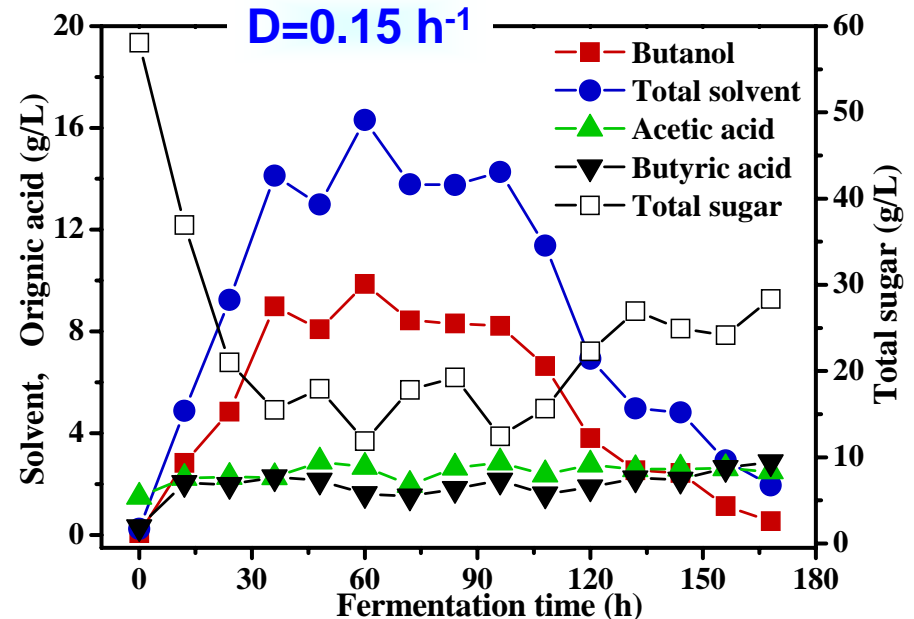
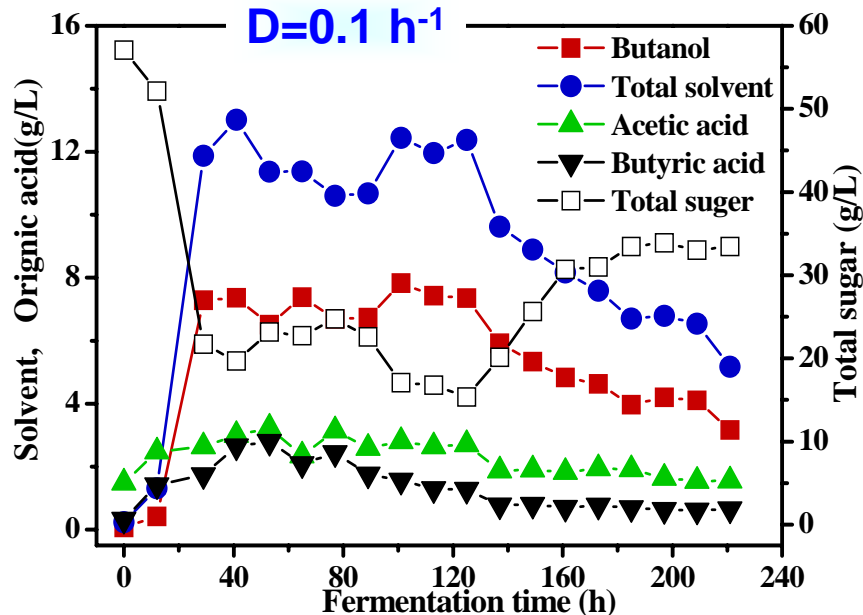
Yield: 0.33 g ABE/g sugar

Fermentation time: 36 h

Substrate: cane molasses

Strain: DSM 13864

4-Stage continuous fermentation



At **D = 0.1 h⁻¹** (30–130 h)

Total solvent: **11.74 g/L** (butanol **7.18 g/L**); Productivity: **0.294 g/L/h**

Fermentation time: 221 h

At **D = 0.15 h⁻¹** (30–100 h)

Total solvent: **13.75 g/L** (butanol **8.37 g/L**); Productivity: **0.439 g/L/h**

Fermentation time: 170 h

Pretreatment conditions of various straw

Straw types	g straw/L liquid	Glucose g/L	Xylose g/L	Arabinose g/L	Total sugar g/L	Enzymolysis ratio %
Corn straw	60	33.34	11.16	1.04	45.54	72.41
	70	42.88	14.32	1.33	58.52	80.51
	80	48.52	16.18	1.59	66.29	80.54
	90	57.19	18.84	2.03	78.06	85.08
Rice straw	60	37.09	11.70	0.65	49.43	78.59
	70	44.00	13.63	0.68	58.30	80.21
	80	49.53	14.71	0.59	64.84	78.78
	90	53.83	17.15	1.59	72.56	79.10
Wheat straw	60	38.34	12.50	0.44	51.27	81.52
	70	45.43	15.74	0.78	61.96	85.23
	80	42.02	14.74	0.83	57.58	69.96
	90	53.16	18.79	1.17	73.12	79.70

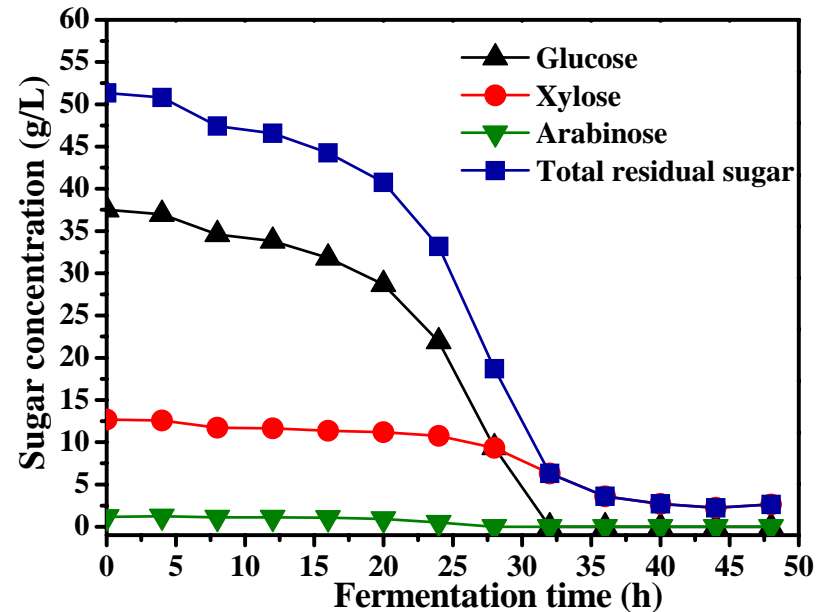
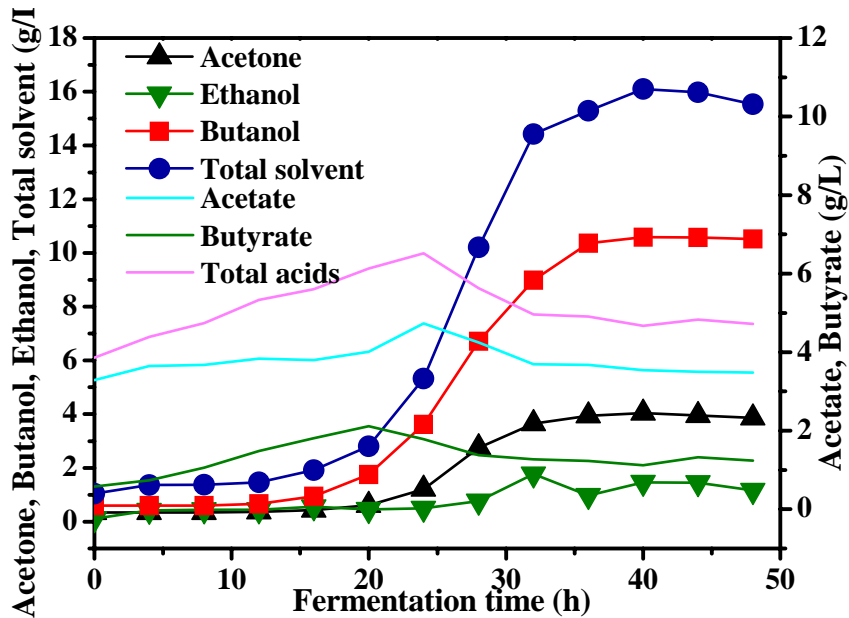
➤ **Alkaline Pretreatment: 1% NaOH, 120 °C for 2 h**

➤ **Cellulase hydrolysis: 20–30 FPIU/g straw, pH 4.8 and 50 °C for 40 h**

Substrate: corn stover hydrolyzate

Strain: DSM 13864

Batch fermentation in 3-L bioreactor



Total solvent: 16.1 g/L (butanol 10.59 g/L)

Productivity: 0.40 g/L/h

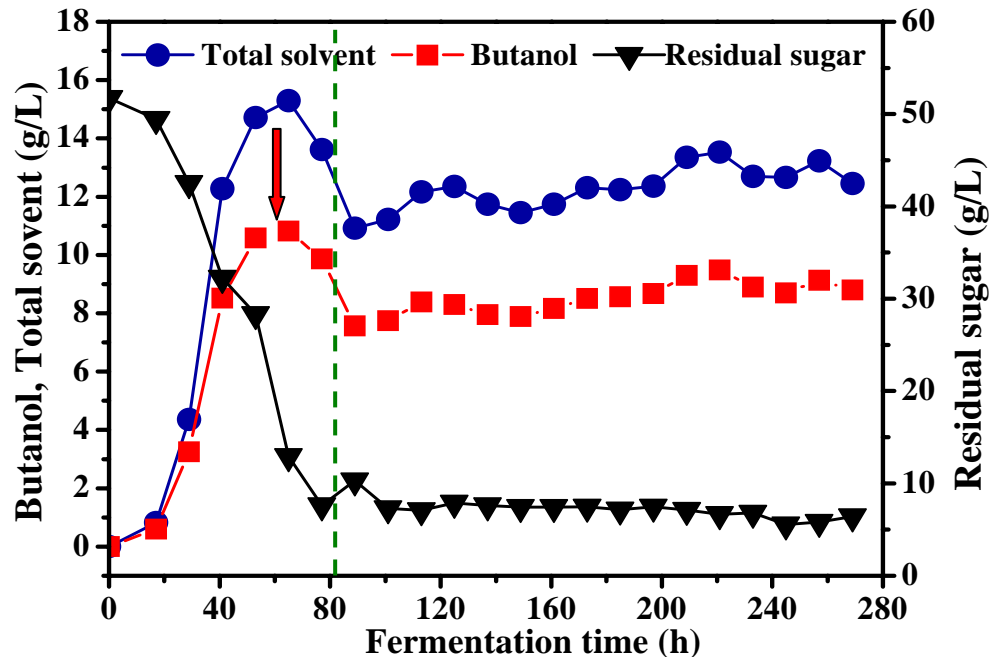
Yield: 0.33 g ABE/g sugar

Fermentation time: 40 h

Substrate: corn stover hydrolyzate

5-stage temperature-shifting continuous fermentation in 500-mL tanks

(Stage 1, 2: 37 °C, Stage 3–5: 30 °C)



Total solvent: 12.28 g/L (butanol 8.50 g/L) after 80 h

Productivity: 0.25 g/L/h

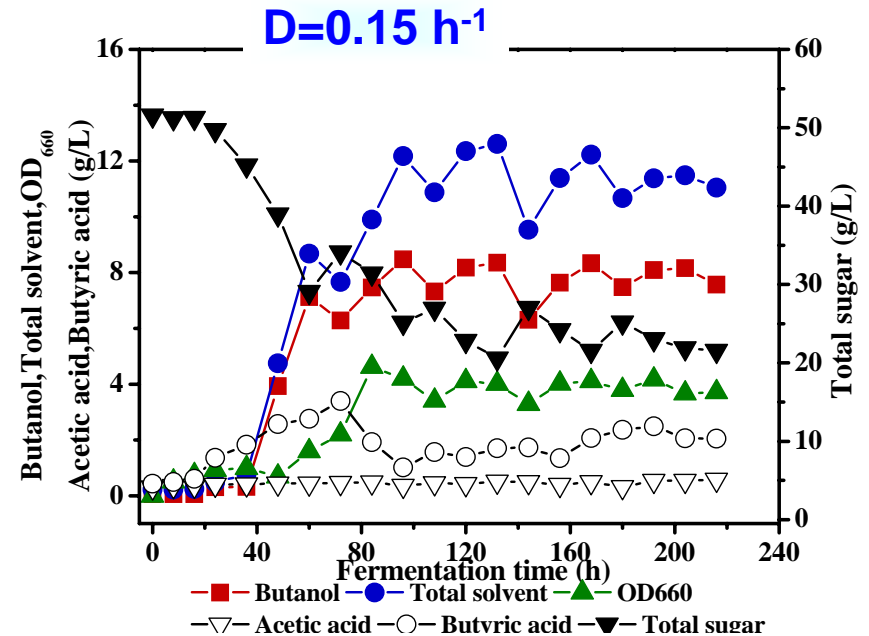
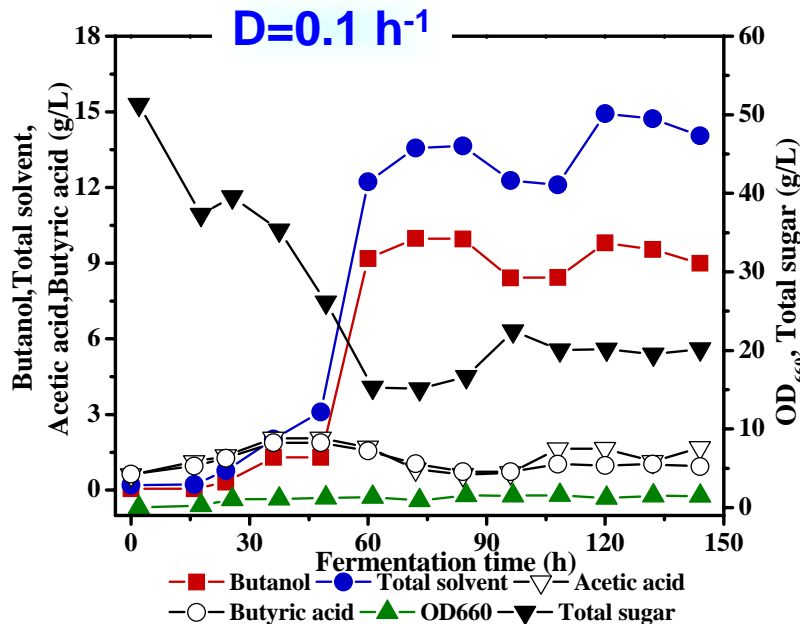
Yield: 0.33 g ABE/g sugar

Fermentation time: 270 h ($D=0.1 \text{ h}^{-1}$)

Substrate: corn stover hydrolyzate

Strain: DSM 13864

4-Stage Continuous fermentation



At **D = 0.1 h⁻¹**

Total solvent: **13.44 g/L (butanol 9.29 g/L)**; Productivity: **0.336 g/L/h**

Fermentation time: 150 h

At **D = 0.15 h⁻¹**:

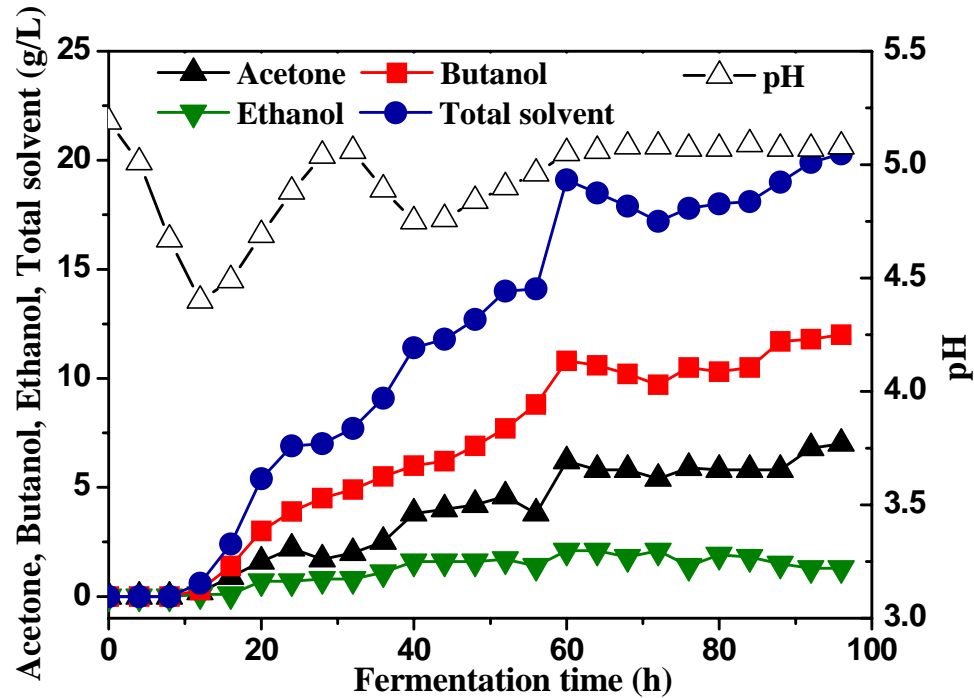
Total solvent: **11.43 g/L (butanol 7.81 g/L)**; Productivity: **0.429 g/L/h**

Fermentation time: 220 h

Substrate: cassava

Strain: *C. acetobutylicum* A

Batch fermentation in 3-L bioreactor



Total solvent: 20.9 g/L (butanol 12.0 g/L)

Productivity: 0.211 g/L/h

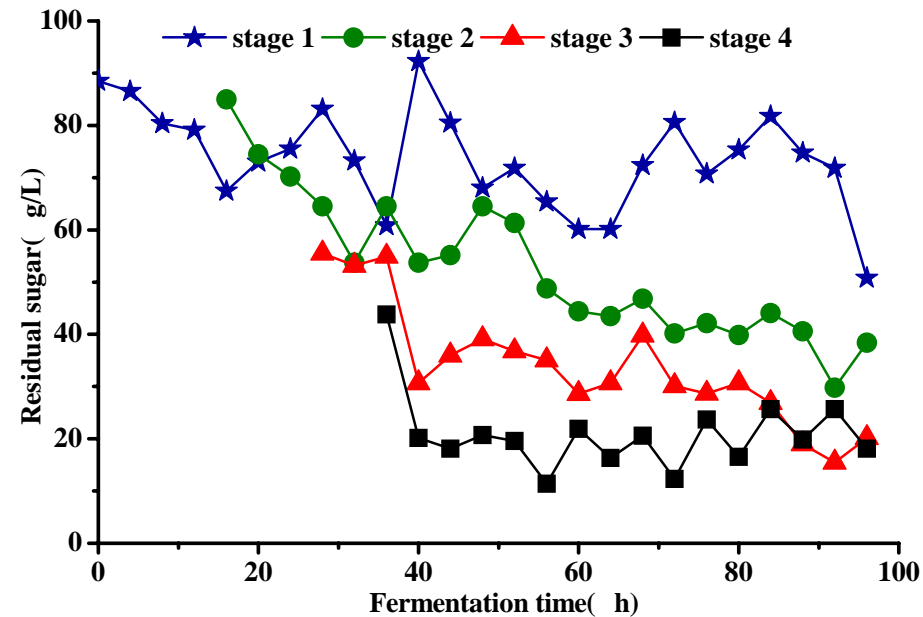
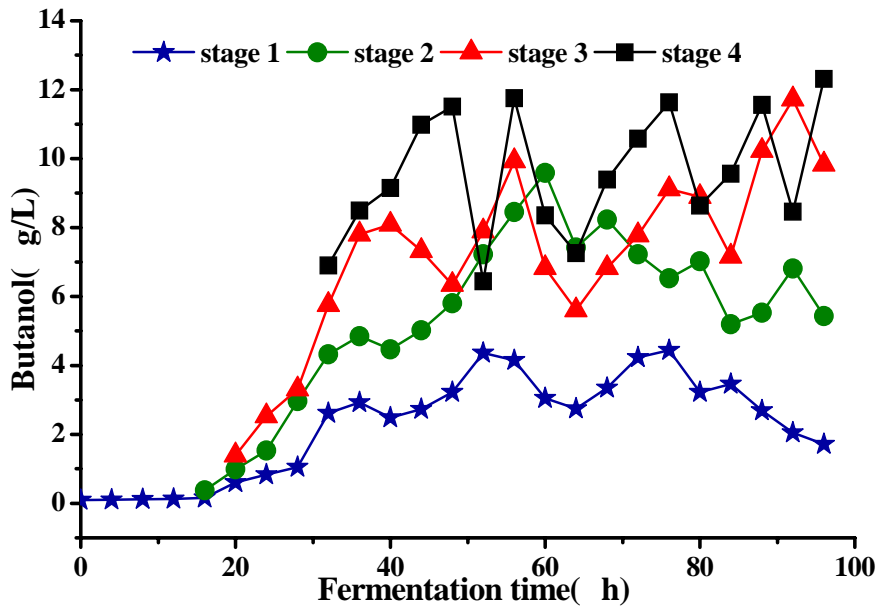
Yield: 0.33 g ABE/g sugar

Fermentation time: 96 h

Substrate: **cassava**

Strain: *C. acetobutylicum A*

4-Stage continuous fermentation in 3-L bioreactor



Total solvent: **22.8 g/L (butanol 12.38 g/L)**

Productivity: **0.57 g/L/h**

Yield: **0.33 g ABE/g sugar**

Fermentation time: **96 h (D=0.1 h⁻¹)**

Discuss

Batch and Continuous ABE fermentation

Operation mode	Strain	Substrate	Dilution rate (h ⁻¹)	Productivity (g/L/h)	Total solvent (g/L)	Reference
Batch Fermentation	<i>C. beijerinckii</i> P260	Corn stover	—	0.31	26.27	Qureshi et al. 2010
	<i>C. acetobutylicum</i> 2N	Beet molasses	—	0.34	16.32	Fan et al. 2010
	<i>C. Saccharobutylicum</i> DSM 13864	Cane molasses	—	0.50	17.88	Ni et al. 2012
	<i>C. acetobutylicum</i> XY16	Glucose	—	0.63	20.30	Guo et al. 2012
Continuous fermentation Immobilized cell	<i>C. beijerinckii</i> BA101	Glucose	2.0	15.80	7.9	Qureshi et al. 2000
	<i>C. beijerinckii</i> ATCC 55025	Glucose	0.2	1.76	8.99	Zhang et al. 2009
Continuous fermentation Membrane cell bioreactor	<i>C. pasteurianum</i> ATCC 6103	Glycerol	0.9	8.3	9.2	Malaviya et al. 2012
	<i>C. Saccharoperbutylacetonicum</i> N1-4	Glucose	0.11	7.55	8.58	Tashiro et al. 2005
Continuous fermentation Free cell	<i>C. saccharobutylicum</i> DSM 13864	Gelatinised sago starch	0.05	0.46	9.10	Liew et al. 2006
	<i>C. acetobutylicum</i> BCRC 10639	Glucose	0.054	0.37	6.85	Yen et al. 2011
	<i>C. saccharobutylicum</i> DSM 13864	Corn stover hydrolysate	0.1 0.15	0.336 0.429	13.44 11.43	Ni et al. Unpublished

Conclusions

- ④ **Low-value sugar-based feedstock** was utilized in batch and continuous ABE fermentation, including: cane molasses, corn stover hydrolyzate, etc.
- ④ Using **cane molasses**, the ABE fermentation could be steadily operated for over 100 h at $D=0.15 \text{ h}^{-1}$, the average **total solvent of 13.75 g/L** (butanol 8.37 g/L); and **productivity of 0.439 g/L/h** were obtained in a 4-stage continuous fermentation.
- ④ **Corn stover hydrolysate** was prepared using alkaline pretreatment and enzyme hydrolysis. In a 4-stage continuous fermentation, the process was operated for **220 h** at $D=0.15 \text{ h}^{-1}$, the **average solvent was 11.43 g/L** (butanol 7.81 g/L), and the average **solvent productivity was 0.429 g/L/h**.

Acknowledgement



Graduate students:

Yun Wang

Ziyi Xia

Gang Song

Shan Sun



Thank you!